

# Reversible interconversion of carbon dioxide and formate by an electroactive enzyme

Torsten Reda\*, Caroline M. Plugge†, Nerilie J. Abram‡, and Judy Hirst\*§

\*Medical Research Council Dunn Human Nutrition Unit, Wellcome Trust/MRC Building, Hills Road, Cambridge CB2 0XY, United Kingdom; †Laboratory of Microbiology, Dreijenplein 10, 6703 HB Wageningen, The Netherlands; and ‡British Antarctic Survey, Natural Environment Research Council, Cambridge CB3 0ET, United Kingdom

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Carbon dioxide (CO<sub>2</sub>) is a kinetically and thermodynamically stable molecule. It is easily formed by the oxidation of organic molecules, during combustion or respiration, but is difficult to reduce. The production of reduced carbon compounds from CO<sub>2</sub> is an attractive proposition, because carbon-neutral energy sources could be used to generate fuel resources and sequester CO<sub>2</sub> from the atmosphere. However, available methods for the electrochemical reduction of CO<sub>2</sub> require excessive overpotentials (are energetically wasteful) and produce mixtures of products. Here, we show that a tungsten-containing formate dehydrogenase enzyme (FDH1) adsorbed to an electrode surface catalyzes the efficient electrochemical reduction of CO<sub>2</sub> to formate. Electrocatalysis by FDH1 is thermodynamically reversible—only small overpotentials are required, and the point of zero net catalytic current defines the reduction potential. It occurs under thoroughly mild conditions, and formate is the only product. Both as a homogeneous catalyst and on the electrode, FDH1 catalyzes CO<sub>2</sub> reduction with a rate more than two orders of magnitude faster than that of any known catalyst for the same reaction. Formate oxidation is more than five times faster than CO<sub>2</sub> reduction. Thermodynamically, formate and hydrogen are oxidized at similar potentials, so formate is a viable energy source in its own right as well as an industrially important feedstock and a stable intermediate in the conversion of CO<sub>2</sub> to methanol and methane. FDH1 demonstrates the feasibility of interconverting CO<sub>2</sub> and formate electrochemically, and it is a template for the development of robust synthetic catalysts suitable for practical applications.

electrocatalysis | formate dehydrogenase | formate oxidation | protein film voltammetry | carbon dioxide reduction

Carbon dioxide (CO<sub>2</sub>) is a kinetically and thermodynamically stable molecule that is difficult to chemically activate. As the unreactive product of the combustion of carbon-containing molecules, such as fossil fuels, and biological respiration, it is accumulating in the atmosphere and is a major cause of concern in climate-change scenarios (1, 2). Consequently, catalysts that are able to sequester CO<sub>2</sub> from the atmosphere rapidly and efficiently, to generate reduced carbon compounds for use as fuels or chemical feedstocks, have long been sought after. Organometallic complexes that insert CO<sub>2</sub> into an M–H bond and the use of supercritical CO<sub>2</sub> to facilitate its hydrogenation are two promising approaches to the development of a homogeneous catalytic process (3–5). Extensive efforts to develop electrode materials for the direct, electrochemical reduction of CO<sub>2</sub> have been made also, but so far, they require the application of extreme potentials (are inefficient energetically) or they are nonspecific and produce mixtures of products (4, 6, 7). An efficient and specific method for reducing CO<sub>2</sub> electrochemically has obvious applications in a future energy economy based on the cyclic reduction and oxidation of simple carbon compounds, as an alternative to the well-known hydrogen economy model.

Here, we focus on the two-electron reduction of CO<sub>2</sub> to formate (see Fig. 1). Formate is the first stable intermediate in the reduction of CO<sub>2</sub> to methanol or methane, but it is increas-

ingly recognized as a viable energy source in its own right. Thermodynamically, formate and hydrogen are oxidized at similar potentials (the reduction potential for the reduction of CO<sub>2</sub> to formate is close to that for the reduction of protons to hydrogen, see below), and fuel cells that use formate are being developed (8). It is not possible, at present, to reduce CO<sub>2</sub> to formate efficiently and specifically at an electrode surface.

Formate dehydrogenases are enzymes that catalyze the oxidation of formate to CO<sub>2</sub>. The most common class catalyze the direct transfer of a hydride moiety from formate to NAD(P)<sup>+</sup>, but it is difficult to drive them in reverse because the reduction potential of NAD(P)<sup>+</sup> is more positive than that of CO<sub>2</sub> (9). In some prokaryotes, however, the formate dehydrogenases are complex enzymes that contain molybdenum or tungsten cofactors to transfer the electrons from formate oxidation to an independent active site, to reduce quinone, protons, or NAD(P)<sup>+</sup> (10–13). These enzymes are suitable for adsorption onto an electrode, so that the electrode accepts the electrons from formate oxidation, and it may also donate electrons and drive CO<sub>2</sub> reduction. Therefore, they are potential electrocatalysts for the reduction of CO<sub>2</sub> (see Fig. 1). Tungstoenzymes catalyze low-potential reactions (14), so tungsten-containing formate dehydrogenases [in which the tungsten is coordinated by two pyranopterin guanosine dinucleotide cofactors and a selenocysteine (12)] are those most associated with CO<sub>2</sub> reduction. Here, we focus on FDH1, one of the tungsten-containing formate dehydrogenases from *Syntrophobacter fumaroxidans*, an anaerobic bacterium that oxidizes propionate to acetate, CO<sub>2</sub>, and six reducing equivalents (15). The reducing equivalents are used to reduce protons to hydrogen or to reduce CO<sub>2</sub> to formate. During syntrophic growth *S. fumaroxidans* optimizes its metabolism by transferring the formate (and/or the hydrogen) to its syntrophic partner (16). Therefore, the tungsten-containing formate dehydrogenases of *S. fumaroxidans* must be both thermodynamically and kinetically efficient, and so they are good candidate electrocatalysts for the electrochemical reduction of CO<sub>2</sub>.

## Results

**Molecular Properties of FDH1 from *S. fumaroxidans*.** FDH1, tungsten-containing formate dehydrogenase 1 isolated from *S. fumaroxidans*, comprises three different subunits [see [supporting information \(SI\) Figs. S1 and S2](#)]. The C-terminal domain of the largest subunit contains the conserved selenocysteine that ligates the tungstopterin active site (17), and it belongs to a large family

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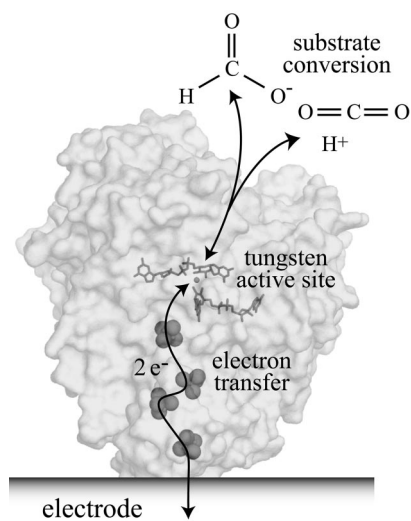
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§To whom correspondence should be addressed. E-mail: [jh@mrc-dunn.cam.ac.uk](mailto:jh@mrc-dunn.cam.ac.uk).

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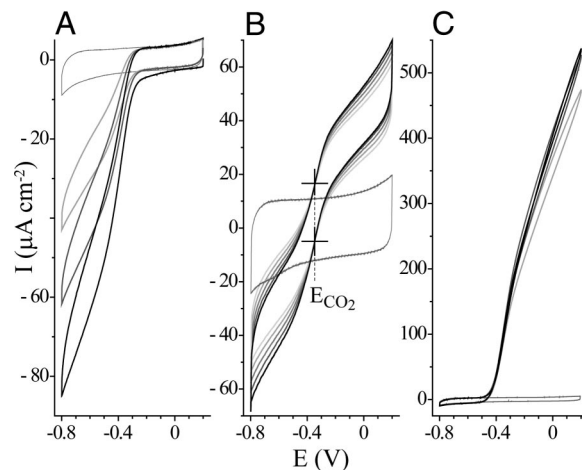
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**Fig. 1.** Schematic representation of the electrocatalytic interconversion of  $\text{CO}_2$  and formate by a formate dehydrogenase adsorbed on an electrode surface. Two electrons are transferred from the electrode to the active site (buried inside the insulating protein interior) by the iron–sulfur clusters, to reduce  $\text{CO}_2$  to formate, forming a C–H bond. Conversely, when formate is oxidized, the two electrons are transferred from the active site to the electrode. The structure of FDH1 (which contains at least nine iron–sulfur clusters) is not known, so the structure shown is that of the tungsten-containing formate dehydrogenase from *Desulfovibrio gigas* [PDB ID code 1H0H (12)].

of structurally related molybdo- and tungstoenzymes, including nitrate reductase (18), DMSO reductase (19), and the structurally characterized formate dehydrogenases (10–12). Between them, the N-terminal domain of the largest subunit and the other two subunits contain binding motifs for at least nine iron–sulfur clusters (see Fig. S2), deduced from their homology to proteins of known structure, in particular three subunits of the hydrophilic domain of respiratory NADH ubiquinone oxidoreductase (complex I) (20). Despite the conservation of residues that bind (or are predicted to bind) the flavin and NADH in complex I, purified FDH1 does not catalyze the reduction of  $\text{NAD(P)}^+$  by formate (15). However, it does catalyze the rapid interconversion of formate and  $\text{CO}_2$  in catalytic activity assays using methyl viologen (MV) as the artificial redox partner; our preparations of FDH1 exhibited turnover rates of up to  $3,380 \text{ s}^{-1}$  for formate oxidation at pH 8, and  $282 \text{ s}^{-1}$  for  $\text{CO}_2$  reduction at pH 7.5. Thus, considering FDH1 as a homogeneous catalyst alone, it exhibits a rate of  $\text{CO}_2$  reduction that is more than two orders of magnitude higher than any known nonbiological catalyst for the same reaction (see below). Note that, for simplicity, we use the term “ $\text{CO}_2$ ” to encompass the pH-dependent equilibrium of dissolved  $\text{CO}_2$ ,  $\text{H}_2\text{CO}_3$ ,  $\text{HCO}_3^-$ , and  $\text{CO}_3^{2-}$  formed in aqueous solution under gaseous  $\text{CO}_2$ , or upon the addition of sodium carbonate (21).

**FDH1 Adsorbed on an Electrode Surface Catalyzes the Reversible Interconversion of  $\text{CO}_2$  and Formate.** Fig. 1 illustrates our experimental strategy (22) for the electrochemical interconversion of  $\text{CO}_2$  and formate. Molecules of FDH1 are adsorbed to a freshly polished pyrolytic graphite edge electrode to activate the surface. When the electrode is placed into an electrochemical cell containing the enzyme’s substrates, catalysis can be driven and controlled by applying a potential and quantified by measuring the current flowing. Thus, the catalytic properties and capability of the adsorbed enzyme are defined under precisely controlled conditions. Ideally, substrate supply to the activated surface and electron transfer between the enzyme’s active site and the



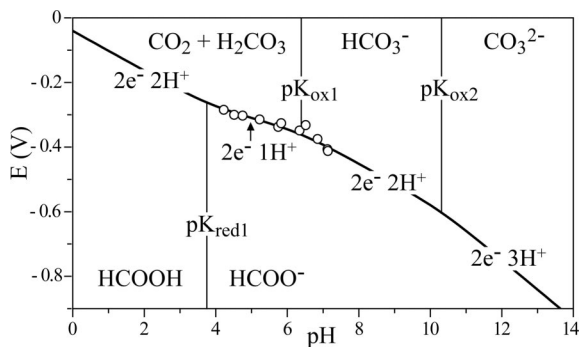
**Fig. 2.** Electrocatalytic voltammograms showing  $\text{CO}_2$  reduction and formate oxidation by FDH1. Shown are the reduction of 10 mM  $\text{CO}_2$  (pH 5.9) (A); electrocatalysis in 10 mM  $\text{CO}_2$  and 10 mM formate (pH 6.4) (B), showing the points of intersection (marked with crosses) that define the reduction potential for the interconversion of  $\text{CO}_2$  and formate; and the oxidation of 10 mM formate (pH 7.8) (C). The first voltammetric cycles are shown in black, subsequent cycles are in gray; background cycles recorded in the absence of substrate are also shown (gray). Note that the background cycle in B is offset slightly from the catalytic scans because of variation in the electrode capacitance. Substrates were added as sodium formate or sodium carbonate. For A and C,  $25 \text{ mV s}^{-1}$ , for B,  $100 \text{ mV s}^{-1}$ ;  $37^\circ\text{C}$ , electrode rotation 1,000 rpm.

electrode are fast and efficient and do not hinder turnover. Fig. 1 highlights how the many iron–sulfur clusters in FDH1 may enable efficient electron transfer through the insulating protein interior to the buried active site.

Voltammograms of FDH1 catalyzing the interconversion of formate and  $\text{CO}_2$  are presented in Fig. 2. Both  $\text{CO}_2$  reduction and formate oxidation are initiated at approximately  $-0.4 \text{ V}$ , close to the reduction potential (see below), and then their rates increase sharply as the driving forces increase. Qualitatively, the voltammograms resemble those exhibited by *Allochromatium vinosum* NiFe hydrogenase, a focus of research in the development of biohydrogen fuel cell technology (23). The voltammetric waveshapes display a sigmoidal onset that changes into a linear dependency as the driving force (overpotential) is increased. This reflects the influence of the interfacial electron transfer process that, even at the highest driving force applied, lags behind the rapid active-site turnover (24).  $\text{CO}_2$  reduction reaches  $0.08 \text{ mA cm}^{-2}$  at  $-0.8 \text{ V}$  (pH 5.9), whereas formate oxidation increases to  $0.5 \text{ mA cm}^{-2}$  at  $+0.2 \text{ V}$  (pH 8.0) (Fig. 2 A and C).

Fig. 2B displays formate oxidation and  $\text{CO}_2$  reduction in a single experiment. The electrocatalytic activity gradually decreases, because of enzyme desorption or denaturation, so that a potential at which all of the catalytic voltammograms intersect is a potential of zero net catalytic current. Net formate oxidation occurs at all potentials above the intersection, and net  $\text{CO}_2$  reduction occurs at all potentials below it. The potentials of zero net catalytic current are the same in both scan directions, and they define the reduction potential for the interconversion of  $\text{CO}_2$  and formate in the solution. Importantly, the current varies continuously across the reduction potential, showing that catalysis is thermodynamically reversible (even the smallest displacement in potential drives turnover) and that the system interconverts electrical and chemical bond energy efficiently.

**The pH-Dependent Reduction Potential of  $\text{CO}_2$ .** Fig. 3 shows how the reduction potential of  $\text{CO}_2$ , measured as the potential of zero net catalytic current in 10 mM  $\text{CO}_2$  and 10 mM formate, varies between pH 4 and pH 8 (the region in which both oxidation and

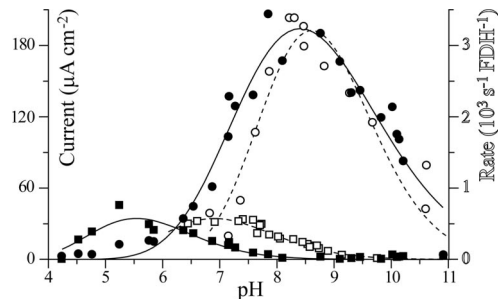


**Fig. 3.** The pH-dependent reduction potential of  $\text{CO}_2$ , measured by using the electrocatalytic voltammetry of FDH1. The reduction potentials (open circle, measured as illustrated in Fig. 2B), were recorded in 10 mM formate and 10 mM  $\text{CO}_2$  at 310 K. They have been fitted to the Nernst equation for the reduction potential of  $\text{CO}_2$  (Eq. 1) by using the parameters  $pK_{\text{red}1} = 3.75$ ,  $pK_{\text{ox}1} = 6.39$ ,  $pK_{\text{ox}2} = 10.32$  (21) and  $E^0 = -0.042$  V. The pH-dependent reduction potential is superimposed on the Pourbaix diagram, showing which species are most stable thermodynamically at different pH values and potentials.

reduction are observed). The data have been fit by using the Nernst equation (Eq. 1). Because the total concentration of solution carbonate species ( $\text{CO}_{2(\text{T})} = \text{CO}_{2(\text{aq})} + \text{H}_2\text{CO}_3 + \text{HCO}_3^- + \text{CO}_3^{2-}$ ) present under 1 atm of  $\text{CO}_2$  increases dramatically at higher pH, Eq. 1 has been calculated by using a closed system containing 1 M  $\text{CO}_{2(\text{T})}$  instead. It includes the  $pK$  values for both the oxidized and reduced states, defined in Fig. 3.

$$E = E^0 - \frac{RT}{2F} \cdot \ln \left\{ \frac{1 + K_{\text{ox}1}/[\text{H}^+](1 + K_{\text{ox}2}/[\text{H}^+])}{1 + K_{\text{red}1}/[\text{H}^+]} \cdot \frac{1}{[\text{H}^+]^2} \right\} \quad [1]$$

The Pourbaix diagram (see Fig. 3) shows that at low pH the pH-dependence reflects the two-electron, one-proton interconversion of  $\text{CO}_2$  (or  $\text{H}_2\text{CO}_3$ ) and formate and, at higher pH, the two-electron, two-proton interconversion of  $\text{HCO}_3^-$  and formate. Thus, the data define an effective  $pK_{\text{ox}1}$  of 6.39 for the equilibrium between  $\text{CO}_2$  (or  $\text{H}_2\text{CO}_3$ ) and  $\text{HCO}_3^-$ , matching the known value (21). The reduction potential at pH 7 is  $-0.389$  V, a value that is consistent with that commonly adopted at neutral pH ( $-0.42$  or  $-0.43$  V, for example, refs. 6 and 25). By using the known value of  $pK_{\text{red}1}$  (3.75) and Eq. 1, the measured reduction potentials extrapolate to  $-0.042$  V at pH 0. Previously, values for the standard reduction potential for  $\text{CO}_2$  to formic acid (pH 0, 1 atm  $\text{CO}_2$ , 289 K) have been calculated from calorimetric data (because irreversible electrochemical responses preclude direct measurements). Perhaps surprisingly, given the current level of interest in  $\text{CO}_2$  reduction, no consensus has been reached, and two different values are quoted,  $-0.199$  V (26) and  $-0.11$  V (4). By using  $34 \text{ mM atm}^{-1}$  for Henry's constant (21), the two standard potentials are redefined as  $-0.157$  V (26) and  $-0.067$  V (4) for 1 M  $\text{CO}_{2(\text{T})}$  instead of 1 atm of  $\text{CO}_2$ . By using the published  $pK$  values (21), they give  $-0.496$  and  $-0.406$  V at pH 7, respectively. The values reported here were recorded under nonstandard conditions, in 10 mM formate and 10 mM  $\text{CO}_{2(\text{T})}$ , at 310 K. They are most consistent with the standard potential of  $-0.11$  V under 1 atm of  $\text{CO}_2$  (equivalent to  $-0.067$  V in 1 M  $\text{CO}_{2(\text{T})}$ ) or  $-0.406$  V at pH 7). Note that experimental measurement of the standard reduction potential is complicated by the highly imperfect behavior of  $\text{CO}_2$  (particularly at high pH) and by the impracticality of measuring at pH 0 by using an enzyme-based system.



**Fig. 4.** The kinetics of catalysis by FDH1 as a function of pH. Electrocatalytic current densities from the first voltammetric scan in 10 mM formate and 10 mM  $\text{CO}_2$  at 0.25 V overpotential (left-hand axis) are compared to data from conventional assays in solution in 10 mM formate or 10 mM  $\text{CO}_2$  (monitored by formation or consumption of the methyl viologen radical, right-hand axis). Lines are guidelines only (dashed lines and open symbols, and solid lines and filled symbols). Open circle, rate of formate oxidation in solution; filled circle, electrocatalytic formate oxidation; open square, rate of  $\text{CO}_2$  reduction in solution; filled square, electrocatalytic  $\text{CO}_2$  reduction.

**Rate of Catalysis by FDH1.** The rate of formate oxidation by FDH1 is greatest at pH 8.4, both in conventional solution assays and on the electrode surface (see Fig. 4). In conventional assays, the rate of  $\text{CO}_2$  reduction increases at lower pH but cannot be measured below pH 6.5 because the absorption coefficient of the MV radical decreases significantly. Electrocatalytic  $\text{CO}_2$  reduction is greatest at pH 5.5. These observations are consistent with  $\text{CO}_2$  being the species that is reduced (rather than  $\text{HCO}_3^-$  or  $\text{CO}_3^{2-}$ ) (27). Direct comparisons of the rates of catalysis in solution and on the electrode are difficult. They may be confounded by kinetic limitations from the artificial redox partner and from interfacial electron transfer, respectively. Furthermore, the amount of electrocatalytically active adsorbed enzyme is too low to be detected in the absence of substrate and may vary with pH. During a 1-hour incubation in a graphite electrocatalysis pot, the total amount of FDH1 that adsorbed to the electrode surface (whether in an electrocatalytically active conformation or not) was estimated from the FDH1 activity lost from solution, and it corresponded to a densely packed monolayer ( $3.7 \pm 0.5 \times 10^{-12} \text{ mol cm}^{-2}$ , calculated value  $3.5 \times 10^{-12} \text{ mol cm}^{-2}$ , assuming a protein density of  $1.4 \text{ g cm}^{-3}$ ). Using the turnover numbers from conventional assays suggests that a monolayer of electrocatalytically active FDH1 should produce limiting current densities of 0.2 mA for  $\text{CO}_2$  reduction at pH 7.5 and 2.4 mA for formate oxidation at pH 8 [comparable with the current density from  $\text{H}_2$  oxidation at either platinum or hydrogenase-modified electrodes (23)]. The maximum current densities observed so far in the voltammetric experiments (as shown in Fig. 2) are significantly lower (0.015 and  $0.5 \text{ mA cm}^{-2}$ , respectively), showing that the number of electrocatalytically active molecules adsorbed on the surface is much lower than that required to constitute a complete monolayer. The low currents observed also reflect the need to optimize the interfacial electron transfer characteristics, to contract the potential-dependent domain and realize the true limiting current.

Importantly, electrocatalytic  $\text{CO}_2$  reduction is observed to increase 6-fold from pH 7.5 to 5.5 (see Fig. 4). The highest current density attained so far in a single experiment ( $0.080 \text{ mA cm}^{-2}$  at pH 5.9 at  $-0.8$  V) corresponds to an average turnover number of  $112 \text{ s}^{-1}$  from a monolayer of FDH1. This value is a known underestimate for the true rate of electrocatalysis by FDH1 (much less than a monolayer of electrocatalytically active enzyme is actually present (see above), and the current at  $-0.8$  V has not achieved its potential independent limit). Nevertheless, it is still more than two orders of magnitude faster than  $\text{CO}_2$  hydrogenation by ruthenium complexes in supercritical  $\text{CO}_2$  (5) and 10 times faster than

**Table 1. Quantitative electrochemical reduction of CO<sub>2</sub> to formate catalyzed by FDH1**

Applied potential, V	Faradaic efficiency, %	Thermodynamic efficiency, %
-0.41	102.1 ± 2.2	96.6
-0.51	98.6 ± 3.6	89.5
-0.61	98.0 ± 1.7	83.4
-0.81	97.3 ± 1.1	73.3

The Faradaic efficiency is the ratio of the formate detected to the charge consumed (accounting for two electrons per formate). The thermodynamic efficiency is the ratio of the chemical bond energy formed ( $E_{\text{H}_2\text{O}} - E_{\text{CO}_2}$ ) to the potential difference applied ( $E_{\text{H}_2\text{O}} - E_{\text{app}}$ ), assuming that the oxidation of H<sub>2</sub>O to O<sub>2</sub> is 100% efficient [ $E_{\text{H}_2\text{O}} = 0.844$  V,  $E_{\text{CO}_2} = -0.368$  V (pH 6.5)]. Experimental conditions: 20 mM sodium carbonate (pH 6.5).

photosynthetic CO<sub>2</sub> activation during the carboxylation of D-ribulose 1,5-bisphosphate by rubisco (28).

**Formate Is the Only Product of CO<sub>2</sub> Reduction by FDH1.** To establish the products of electrochemical CO<sub>2</sub> reduction by FDH1, a graphite “pot” working electrode was used for bulk electrocatalysis. FDH1 was adsorbed from the solution [containing 20 mM sodium carbonate (pH 6.5)] during electrocatalysis. This method sustained a small population of adsorbed electroactive molecules but provided a lower maximum current (typically 15  $\mu\text{A cm}^{-2}$  after 15 min.) than direct application of a concentrated solution. The overpotential and time of electrocatalysis were varied; typically, in a 1-hour experiment the current at -0.8 V averaged 8.5  $\mu\text{A cm}^{-2}$  (30.4  $\text{mC cm}^{-2} \text{h}^{-1}$ ), and the FDH1 molecules present catalyzed, on average, 42,500 transformations. The total charge passed was defined by integrating the current-time curve, and the formate produced was quantified by ion-exclusion chromatography. The data (see Table 1) reveal that formate is the sole product of electrocatalytic CO<sub>2</sub> reduction by FDH1, with a measured Faradaic efficiency of  $\approx 100\%$  at modest overpotentials. At higher overpotentials, the efficiency decreases slightly (to 97% at 0.45 V overpotential) because nonspecific electrode reactions begin to contribute.

## Discussion

There have been many attempts to drive the electrochemical reduction of CO<sub>2</sub> to formate (4, 6, 7). However, excessive overpotentials were required so that a significant proportion of the potential applied was dissipated as heat. Furthermore, mixtures of products were formed, resulting from the formation of the CO<sub>2</sub><sup>-</sup> radical and from competing reactions such as hydrogen formation. Notably, the direct reduction of aqueous CO<sub>2</sub> at lead, mercury, indium, and thallium electrodes produces formate with >90% Faradaic efficiency but only at potentials below -1.5 V. Table 1 reports the “thermodynamic efficiency” of CO<sub>2</sub> reduction (coupled to H<sub>2</sub>O oxidation) at the overpotentials used here. For comparison, at -1.5 V,  $\approx 50\%$  of the potential is dissipated as heat. Preliminary attempts to use a ruthenium catalyst to reduce CO<sub>2</sub> to formate electrochemically required similarly high overpotentials and also led to a mixture of products (29). Formate dehydrogenase from *Pseudomonas oxalaticus* was applied also to the electrochemical reduction of CO<sub>2</sub> (25). However, it was present in solution at high concentration, and electron transfer between the enzyme and the electrode was mediated by millimolar concentrations of methyl viologen (comparable with the concentrations of formate generated), with variable Faradaic efficiency. The only previous demonstration of efficient electrocatalytic CO<sub>2</sub> reduction is from another adsorbed enzyme, CO dehydrogenase I from *Carboxydotherrmus hydrogenoformans*, which catalyzes the rapid and

reversible interconversion of CO<sub>2</sub> and CO (not CO<sub>2</sub> and formate) (30).

Virtually nothing is known about the mechanism of CO<sub>2</sub> activation and reduction in enzymes such as FDH1. A number of rudimentary bis(dithiolene)tungsten<sup>IV,VI</sup> thiolate and selenolate compounds have been synthesized to mimic the active sites of formate dehydrogenases (31), but, perhaps unsurprisingly, they exhibit no catalytic activity. However, although molybdenum and tungsten are not generally associated with biological hydride transfer reactions (14, 32), CO<sub>2</sub> is known to insert into the W-H bond in [HW(CO)<sub>5</sub>]<sup>-</sup> to form a stable formate adduct (33), and considerable progress has been made in developing homogeneous organometallic catalysts based on M-H insertion reactions (3, 4). For example, CO<sub>2</sub> insertion into Ru(terpy)(bpy)H<sup>+</sup> proceeds at 8.5 s<sup>-1</sup> in 10 mM CO<sub>2</sub> (although displacement of the formate by H<sub>2</sub>O to complete a catalytic cycle is significantly slower) (34).

FDH1 is the first example of a molecular structure that can activate an electrode to reduce CO<sub>2</sub> (and form a C-H bond) specifically, rapidly, reversibly, and under thoroughly mild conditions. Although, as a large and oxygen-sensitive protein complex it is not itself a realistic target for technical exploitation, FDH1 establishes an important paradigm. It is accessible to electrochemical, spectroscopic and structural studies, to provide detailed mechanistic information and elucidate structure-function relationships. It is hoped that these will aid in the rational evaluation and development of robust synthetic compounds that host similar chemical and electrochemical capabilities to FDH1 and that would be suitable for future applications in carbon capture, energy storage, and fuel cell devices.

## Materials and Methods

All procedures were carried out under strictly anaerobic conditions. FDH1 was isolated from *S. fumaroxidans* cells grown on 20 mM propionate and 60 mM fumarate by using the protocol described (15) with minor modifications, except that FDH1 eluted from the hydroxyapatite column (40  $\mu\text{m}$  type II CHT ceramic; Bio-Rad) in a linear gradient of sodium phosphate (pH 7). In conventional activity assays at 37°C, oxidation was initiated by 10 mM sodium formate, after a 2-min incubation of FDH1 in 1 mM MV, 10  $\mu\text{M}$  dithionite, 50 mM Tris-Cl (pH 8), and reduction was initiated by adding 10 mM sodium carbonate to FDH1 in 100 mM sodium phosphate (pH 7.5), 0.1 mM MV, 0.045 mM dithionite. The reactions were followed spectrometrically by the reduction of MV or by the oxidation of the MV radical, respectively ( $\epsilon_{578} = 9.7 \text{ mM}^{-1} \text{ cm}^{-1}$ ). pH values were checked after experimentation.

Cyclic voltammetry was performed at 37°C as described (24), by using a rotating disk pyrolytic graphite edge (PGE) electrode. pH was controlled by using a mixed-buffer system [10 mM potassium acetate, 2-morpholinoethane sulfonic acid (Mes), *N*-cyclohexyl-2-aminoethane sulfonic acid (Hepes), and *N*-tris(hydroxymethyl)methyl-3-aminopropanesulfonic acid (TAPS)] and checked following experimentation. All potentials are reported relative to the standard hydrogen electrode. Electrocatalysis was carried out at 25°C in 100 mM Mes (final pH 6.5), 1 M NaCl, 20 mM sodium carbonate, and  $\approx 5 \mu\text{g}$  FDH1, in a PGE pot working electrode (0.75 ml, surface area 3.94 cm<sup>2</sup>) and monitored amperometrically. The Ag/AgCl reference electrode and platinum mesh counter electrode were behind a Vycor glass frit. Formate concentrations were determined by ion-exclusion chromatography (using a Dionex AS15 column (2 × 250 mm), IonPac AG15 guard column (2 × 50 mm), and suppressed-conductivity ICS-2000 detector). Formate was eluted isocratically in 20 mM KOH, and concentrations >0.25 ppm (5.4  $\mu\text{M}$ ) were determined with a standard deviation of 0.5%.

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